# Effects of stretch and thermal radiation on difluoromethane/air burning velocity measurements in constant volume spherically expanding flames\*

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# Effects of stretch and thermal radiation on difluoromethane/air burning velocity measurements in constant volume spherically expanding flames

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#### **Abstract**

Compared to current refrigerants, next-generation refrigerants are more environmentally benign but more flammable. The laminar burning velocity is being used by industry as a metric to screen refrigerants for fire risk, and it is also used for kinetic model development and validation. This study reports measurements of difluoromethane/air flame burning velocities for equivalence ratios from 0.9 to 1.4 in a spherical, constant volume device. Experimental burning velocities produced with the aid of an optically thin radiation model are about 17 % greater than those obtained with an adiabatic model. Characterization of flame stretch based on the product of Markstein and Karlovitz numbers indicates that while many experimental data are nearly stretch-free, those for slower burning velocities, smaller flame radii, and leaner conditions may not be. Limiting the data to regions estimated to be stretch-free requires extrapolation away from the experimental conditions to extract burning velocities near ambient conditions, e.g., at (298 K, 101 kPa). Lower uncertainty, desirable for kinetic model validation, is obtained by interpolating between experimental conditions, e.g., at (400 K, 304 kPa). Since thermal radiation and flame stretch were found to affect the inferred burning velocities of difluoromethane/air constant volume spherical flames, they should also be considered during data reduction of other mildly flammable refrigerants.

# **Keywords:**

Refrigerant flammability, burning velocity, difluoromethane, thermal radiation, flame stretch

### 1. Introduction

Due to their high global warming potential (GWP), hydrofluorocarbon refrigerants in vaporcompression equipment are being phased down [1]. Replacement compounds with lower GWP are being
developed, but the properties that allow them to react in the troposphere and maintain low GWP (typically
adding H atoms or double carbon bonds) also make them mildly flammable. Flammable refrigerants are
a new concern for the heating, ventilating, air-conditioning and refrigerating (HVAC&R) industry;
characterizing the fire risk of these new agents is of high interest and the subject of recent study (e.g., [2]).
There is a need to both rank the flammability of new agents and understand their full-scale fire behavior.
The HVAC&R industry has adopted the burning velocity ( $S_u$ ) as one flammability metric [3], which is
reasonable since  $S_u$  affects flame stabilization, the rate of pressure rise in confined flame propagation, and
is used in turbulent premixed combustion models.

Industry has an urgent need for a reliable  $S_u$  screening method for refrigerant/air flames. Defining such a method is made more challenging by the low  $S_u$  values for the refrigerant/air flames of interest, often between 1 cm/s to 10 cm/s. The American Society of Heating, Refrigerating and Air-Conditioning Engineers (ASHRAE) Standard 34 [3] specifies flammability Class 2L based on measured  $S_u$  less than 10 cm/s. These flames propagate at slow speeds similar to those of near-limit methane/air flames despite producing high flame temperatures similar to stoichiometric methane/air flames.

Difluoromethane (R-32, CH<sub>2</sub>F<sub>2</sub>) exhibits prototypical refrigerant/air flammability behavior and is selected for study in the present work. It is used as a pure working fluid or in blends, e.g., R410A is a 50/50 mass blend of R-32 and R-125 (C<sub>2</sub>HF<sub>5</sub>). The 100-year GWP of R-32 (GWP = 677) is lower than R-125 (GWP = 3170) but higher than R-1234yf (CH<sub>2</sub>CFCF<sub>3</sub>, GWP < 1) [4]. A peak  $S_u$  for R-32/air flames at ambient conditions is currently defined to be 6.7 cm/s in the ASHRAE flammability standard [3]. Thus, it is important to have accurate CH<sub>2</sub>F<sub>2</sub>/air  $S_u$  measurements.

The present experimental approach employs outwardly propagating spherical flames in a constant volume device with  $S_u$  calculated from the measured pressure rise and a thermodynamic flame model (e.g., [5-10]). Other methods used with refrigerants include: flame propagation in a vertical tube [11, 12]; constant pressure method outwardly propagating spherical flames (e.g., [13, 14]); and steady flow, nozzle-stabilized flames (e.g., [15]). Each has advantages and disadvantages as a standard test method. For instance, the tube method is subject to unquantified buoyancy, wall, and stretch effects [16]. The nozzle burner cannot be used for low burning velocities and consumes large quantities of reactants. The constant pressure spherical flame method requires relatively expensive optical equipment. The constant volume spherical flame method (e.g., [10]) uses small quantities of reactants, produces little product gas (which can contain up to 30 % HF by volume in  $CH_2F_2$ /air flames), and requires relatively inexpensive equipment. Spherically expanding flames are widely used to measure  $S_u$  of hydrocarbon/air mixtures for which the effects of buoyancy (e.g., [13, 17]), thermal radiation (e.g., [18-22]), and flame stretch (e.g., [20, 21, 23-26]) have been recent topics of research.

An important additional use for experimental burning velocity data is for kinetic model development and validation (e.g., [27]). For this purpose, it is the convention to use the laminar burning velocity ( $S_u^0$ ) defined as the propagation speed into unburned reactants of a flame that is adiabatic, laminar, one-dimensional, steady, and stretch-free [28]. Small experimental uncertainty in  $S_u^0$  is needed to properly constrain kinetic model rate parameters.

The present work investigates the role of radiation and stretch on the values of  $S_u$  and  $S_u^0$  determined in spherical, constant volume method  $CH_2F_2$ /air flames. Using both constant volume and constant pressure spherical flame methods, Takizawa et al. [13] found that, for stoichiometric or rich flames, normal and micro-gravity  $CH_2F_2$ /air flame propagation measurements agree for values of  $S_u^0 > 5$  cm/s. Since all  $S_u^0$  values presently measured exceed this limit, buoyancy was not further considered.

# 2. Experimental approach

Measurements were performed using the 15.14 cm inner diameter stainless steel spherical chamber described in Refs. 7 and 8. Reactants were  $CH_2F_2$  (Honeywell, Genetron 32, 99.9 % purity), argon (Messer Group, 99.995 % purity), oxygen (Air Products, 99.5 % purity), and house air treated with a 0.01  $\mu$ m filter, a carbon filter, and a desiccant bed to remove small aerosols, organic vapors, and water vapor; final relative humidity in the air was typically less than 2 % [8]. After evacuating the chamber to less than 67 Pa for at least 5 minutes, reactants were added via partial pressures using an absolute pressure transducer (Omega PX811) calibrated against a heated absolute pressure capacitance manometer (Baratron 627D) with a reading accuracy of 0.12 %. Mixture initial temperature ( $T_i$ ) was between 295 K and 299 K, and initial pressure ( $P_i$ ) was between 87.9 kPa (660 torr) and 115 kPa (860 torr). Mixtures were given 5 minutes to settle and were then centrally ignited by a spark powered by a 100 nF capacitor bank charged to 13 kV. Pressure rise in the chamber was measured at 20 kHz using a piezoelectric pressure sensor (PCB Piezotronics 101A06) with a resolution of 0.07 kPa, a range of 3450 kPa, and a claimed accuracy of ±3.5 kPa.

Previous uncertainty analysis for this experimental system [8] suggests relative uncertainties in the initial mixture of about 1 % in the fuel/air equivalence ratio ( $\phi$ ), and 0.3 % and 0.8 % in the partial pressure of air and CH<sub>2</sub>F<sub>2</sub>, respectively. Relative uncertainty was 1.3 % in the dynamic pressure rise, 0.7 % in  $P_i$ , and 1 % in  $T_i$ . The maximum combined relative uncertainty at low  $S_u$  for a single experimental  $S_u$  measurement is  $\pm 12$  %.

### 3. Data reduction

Inferring  $S_u$  from a measured pressure (P) - time (t) trace employs the data reduction procedures summarized in Fig. 1. First, P(t) is measured and noise is suppressed with cubic smoothing splines selected to ensure unstructured fit residuals over the useful range of data. The range of smoothed P(t) is narrowed: data at early times are eliminated for  $P(t) < 1.25P_i$ , which is sufficient to remove ignition transients and electrical noise; data at longer times are eliminated beyond the maximum  $2^{nd}$  derivative of the pressure trace, which has been suggested as a marker for when the flame begins to interact with the chamber walls [29]. Second, the relationship between the unburned/burned gas thermodynamic states and the flame radius  $(R_f)$  was computed via the Hybrid ThermoDynamic-Radiation (HTDR) model [9] with species thermodynamic data taken from the NIST HFC mechanism [30]. Finally, the measured P(t) and modeled  $R_f(P)$  are combined to reconstruct  $S_u$  and the flame stretch rate (K).

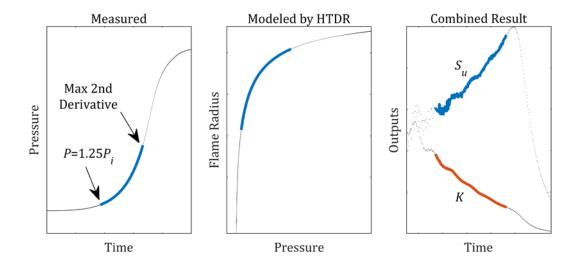


Figure 1: Data reduction process. A measured pressure trace (left) is smoothed, cropped, and combined with (center) the modeled flame radius to generate (right) flame burning velocity and stretch rate.

HTDR is a numerical, multi-zone, thermodynamic, spherically expanding flame model [9] which includes thermal radiation calculations based on RADCAL [31]. It assumes that the flame front is smooth, spherical, and infinitely thin; that no reactions occur in the unburned gas, which has uniform temperature

and composition; that the pressure is spatially uniform but evolves in time; that the unburned gas compression occurs isentropically; and that the burned gas is in chemical equilibrium at any instant. The model works by dividing the spherical domain into a series of shells and applying conservation of energy, mass, and volume. Starting from the center, an unburned shell is combusted by allowing it to reach equilibrium at constant pressure and enthalpy, causing increased volume and temperature. Equilibrium is then re-computed for all inner (burned) shells. Next, if radiation is enabled, all burned shells radiate at constant pressure, causing decreased volume and temperature. Finally, all shells are simultaneously, isentropically compressed to match the chamber volume. From this, the functional relationship for flame radius  $R_f(P)$  is obtained.

From the measured P(t) and modeled  $R_f(P)$ , the inferred  $S_u$  is calculated based on the result of Fiock and Marvin for a constant volume spherically expanding flame [32]:

$$S_{u} = \frac{dR_{f}}{dt} - \frac{(R_{w}^{3} - R_{f}^{3})}{3R_{f}^{2}\gamma_{u}P} \frac{dP}{dt}$$
 (1)

where  $\gamma_u$  is the unburned gas specific heat ratio and  $R_w$  is the chamber radius. Using the chain rule,  $\mathrm{d}R_f/\mathrm{d}t$  is evaluated via the product  $(\mathrm{d}R_f/\mathrm{d}P)(\mathrm{d}P/\mathrm{d}t)$ . The terms in Eq. (1) can be defined as  $S_u=S_f-S_g$ , which shows that  $S_u$  is computed from the difference of the total flame front velocity relative to the chamber center point  $(S_f=\mathrm{d}R_f/\mathrm{d}t)$  and the velocity due to gas expansion from heat release  $(S_g)$ .

At each equivalence ratio  $(\phi)$  tests were conducted at multiple  $P_i$  (typically three) between 87.9 kPa and 115 kPa. Each test is assumed to evolve in time along an isentrope in  $(T_u, P)$  space, where  $T_u$  and P are the unburned gas temperature and pressure, and  $S_u$  is obtained from Eq. (1). As done in the past (e.g., [33]), the experimental  $S_u$  curves are fitted with a power law surface  $(\widehat{S_u})$  of the form:

$$\widehat{S_u}(T_u, P) = S_{u,ref} \left(\frac{T_u}{T_{ref}}\right)^a \left(\frac{P}{P_{ref}}\right)^b \tag{2}$$

where  $S_{u,ref}$  is the value of surface  $\widehat{S}_u$  at a reference state  $(T_{ref}, P_{ref})$  and the exponents a and b are determined during fitting. Figure 2 shows the three experimental  $S_u$  curves, corresponding  $\widehat{S}_u$  surface fit,

and projections of  $S_u$  on each coordinate plane for CH<sub>2</sub>F<sub>2</sub>/air with  $\phi=1.1$ , assuming adiabatic conditions in the burned gas. Each  $S_u$  curve corresponds to one measured P(t) trace with  $P_i=87.9$  kPa, 101 kPa, or 115 kPa. Using the surface fit  $\widehat{S_u}$ , values for  $S_u$  can be obtained at arbitrary  $(T_u, P)$ , not just along the measured isentropes. For example, Fig. 2 shows, in the  $(T_u, P)$  plane, the locations of the two states, (298 K, 101 kPa) and (400 K, 304 kPa), for which experimental  $S_u^0$  values are reported in the present work. Caution is advised when selecting  $(T_u, P)$  which require extrapolation far from the experimental isentropes as additional uncertainty will be introduced. For example,  $\widehat{S_u}(298 \text{ K}, 101 \text{ kPa})$  in Fig. 2 is an extrapolation over about 30 K and 25 kPa but  $\widehat{S_u}(400 \text{ K}, 304 \text{ kPa})$  is an interpolation between  $P_i = 87.9$  kPa and 101 kPa experimental isentropes.

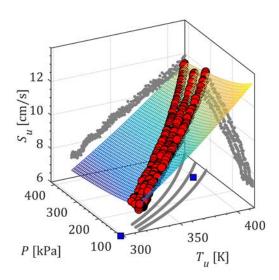


Figure 2: Example data set and fitted power law surface for  $CH_2F_2$ /air at  $\phi = 1.1$ . Experimental  $S_u$  curves are marked as red circles and their 2D projections in each coordinate plane as grey dots. Fitted  $\widehat{S_u}$  is shown as a mesh surface. Reference states (298 K, 101 kPa) and (400 K, 304 kPa) are marked on the  $(T_u, P)$  plane as blue squares.

Thermal radiation affects spherically expanding flames in two ways [18]. Reduced temperatures within the reaction zone cause lower reactivity and reduced  $S_u$ . Also, the hot product gases radiating heat will contract as their mass density increases, causing the flame to propagate against a radially inward flow. RADCAL provides various models to account for radiation: adiabatic conditions (no radiation correction),

emission-only radiation at the optically thin limit without reabsorption, or optically thick narrow-band radiation with reabsorption. Calculation of narrow-band radiation emission/absorption is computationally expensive and requires parameters not well characterized for the species present in  $CH_2F_2$  combustion. Therefore,  $R_f(P)$  was modeled only for adiabatic and optically thin conditions with the understanding that results of the more rigorous reabsorption radiation model fall between these limits [22]. RADCAL already contains Planck mean absorption coefficients for CO,  $CO_2$ ,  $H_2O$ , and  $CH_4$ , and values for HF as a function of temperature [34] were added.

Besides radiation, another major factor that can affect  $S_u$  is flame stretch. Williams [35] estimated the stretch rate in spherically expanding flames as  $K = (2/R_f)(\mathrm{d}R_f/\mathrm{d}t)$ . A nondimensional form of K is the Karlovitz number,  $Ka = (\alpha/S_u^2)K$ , where  $\alpha$  is the mixture thermal diffusivity. In spherically expanding laminar flames, Ka is greatest at small  $R_f$  where the flame surface is strongly curved. In constant volume method flames, the rising pressure reduces  $\alpha$  which also helps drive  $Ka \to 0$  for larger  $R_f$  (e.g., [9]). If stretch affects the measured  $S_u$ , it is expected to be most prominent at smaller  $R_f$ .

Positive stretch in spherically expanding flames is known to impact  $S_u$  in two ways: through imbalanced diffusive flux of thermal energy leaving the flame compared to chemical enthalpy entering, called preferential diffusion, and through a  $\phi$  shift caused by faster transport of the more mobile reactant into the flame, called differential diffusion [28]. Preferential diffusion is parameterized by the Lewis number ( $Le = \alpha/D$ ) which is the ratio of a gas mixture's thermal diffusivity to mass diffusivity (D). For  $CH_2F_2$ /air flames, Le > 1 such that as stretch increases the flames diffuse heat away at a greater rate than chemical enthalpy is gained leading to reduced flame temperatures and  $S_u$ . Preferential diffusion causes a lean shift in  $CH_2F_2$ /air flames due to the lower mobility of  $CH_2F_2$  compared to  $O_2$ .

Lewis number effects are reflected in the Markstein length  $(\mathcal{L})$  which is nondimensionalized by the flame thickness  $(\delta_f)$  to form a Markstein number  $(Ma = \mathcal{L}/\delta_f)$  for which  $|Ma| \gg 0$  corresponds to flames with high sensitivity to stretch. A previous study [14] suggests that Ma is large and positive for lean

CH<sub>2</sub>F<sub>2</sub>/air flames, which exhibit a strong stretch response, and that Ma approaches zero in rich flames which exhibit weak stretch response. It is possible to calculate Ma values based on simplified theoretical models (e.g., [36]), but these values are expected to be instructive rather than accurate due to the simplifications and uncertainties involved. To estimate Ma values for CH<sub>2</sub>F<sub>2</sub>/air flames, computed values for C<sub>3</sub>H<sub>8</sub>/air mixtures were used as approximations (justified based on the comparable molecular weights of CH<sub>2</sub>F<sub>2</sub> and C<sub>3</sub>H<sub>8</sub>). Although this constitutes a significant approximation, an uncertainty factor of 2 was assigned to Ma for the purposes of evaluating the sensitivity of results to presumed Ma values. This uncertainty factor was chosen to encompass Ma values computed by Matalon [36] for flames in air with a variety of fuel molecule types and molecular weights, from methanol to octane.

Knowing Ka and Ma, the effect of stretch in  $S_u$  measurements can be evaluated. For sufficiently small stretch rates,  $S_u = S_u^0 - \mathcal{L}K$  [36], or in non-dimensional parameters:

$$S_u = \frac{S_u^0}{1 + MaKa} \tag{3}$$

such that  $CH_2F_2/air$  flames characterized by  $MaKa \ge 0$  have  $S_u \le S_u^0$  while stretch-free flames characterized by  $MaKa \approx 0$  produce  $S_u \approx S_u^0$ . Note that Eq. (3) suggests, in principle, that measured  $S_u$  can be corrected to recover unstretched  $S_u^0$  for a given MaKa. In practice, MaKa is not known with enough certainty to justify this approach. In the present work, an empirical tolerance of  $MaKa \le 0.005$  was selected for  $S_u \approx S_u^0$ , which imposed an additional constraint on the useable range of P(t) relevant for stretch-free conditions.

### 4. Results and discussion

The inferred experimental  $S_u$  values are sensitive to the choice of radiation model used in data reduction. This is demonstrated on the left frame of Fig. 3 for experimental  $S_u$  values of  $CH_2F_2$ /air flames with  $\phi = 1$  and  $P_i = 101$  kPa. Values obtained assuming optically thin radiation in the burned gas are about 17 % greater than those assuming adiabatic conditions. As described previously [22], the results with narrow-band radiation fall between these two limits. Given the significant correction illustrated in Fig. 3, data reduction using a narrow-band radiation model is warranted, however, the required radiation parameters are not available for halogenated hydrocarbon species under combustion conditions.

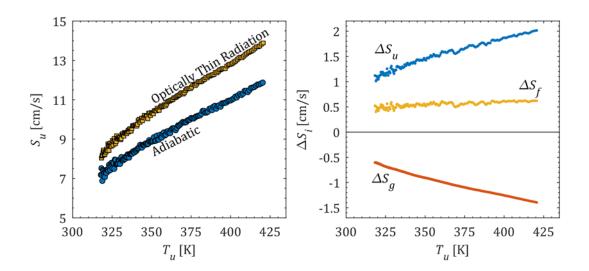


Figure 3: (Left) Comparison of experimental  $S_u$  values with and without thermal radiation for CH<sub>2</sub>F<sub>2</sub>/air at  $\phi = 1$  and  $P_i = 101$  kPa. (Right) Component contributions to the total difference in  $S_u$ .

The reasons for the strong radiation effect are explored based on the terms of Eq. (1), i.e.,  $S_u = S_f - S_g$ , in the right frame of Fig. 3. The total difference between  $S_u$  obtained using the optically thin and adiabatic models ( $\Delta S_u$ ) is decomposed into differences between total flame front velocity ( $\Delta S_f$ ) and gas expansion velocity ( $\Delta S_g$ ), i.e.,  $\Delta S_u = \Delta S_f - \Delta S_g$ . Since the optically thin values are greater than the adiabatic ones,  $\Delta S_u$  is positive for the present example, and of magnitude between 1 cm/s and 2 cm/s.

The greatest contribution is from  $\Delta S_g$  which accounts for about 0.5 cm/s to 1.5 cm/s of the total difference, but at smaller  $R_f$  (i.e., low  $T_u$ ) it is nearly matched in magnitude by  $\Delta S_f \approx 0.5$  cm/s. The burned gas thermal radiation influences the inferred  $S_u$  through reduced burned gas expansion velocity and greater total flame front velocity.

The impact of flame stretch on  $S_u$  should also be considered during data reduction, so that stretched flames are not included in the data reduction for  $S_u^0$ . Experimental values of  $S_u$  as a function of  $T_u$ , assuming adiabatic conditions, for CH<sub>2</sub>F<sub>2</sub>/air flames with  $P_i = 101$  kPa and  $\phi = 0.9$  and 1.3 are shown in Fig. 4 (left frame). In lean CH<sub>2</sub>F<sub>2</sub>/air flames, both differential and preferential diffusion cause reduced flame temperatures. In rich flames, the lean shift caused by preferential diffusion strengthens the flame and counteracts, to some extent, the weakening due to differential diffusion. These trends are illustrated in Fig. 4 (left frame), which shows that a greater range of rich flame data meets the empirical stretch-free criterion ( $MaKa \le 0.005$ ) than does lean flame data. For rich flames, about 2/3 of the data (corresponding to T > 350 K) meet the stretch-free criterion, however, the power law fit to only "stretch-free" data also follows the remaining 1/3 of the data at lower  $T_u$ . Similar results were found for stoichiometric flames (not shown in Fig. 4). For lean flames, only about 1/4 of the data (i.e.,  $T_u > 365$  K) meet the stretch-free criterion and the resulting power law fit to those "stretch-free" data overshoots the measurements at lower  $T_u$  by about 12 % at 315 K. Thus, for the lean flames, the surface fit parameters are sensitive to the choice of MaKa threshold which results in additional uncertainty, especially when extrapolating far from the valid range of stretch-free data, e.g., to 298 K and 101 kPa. Moreover, power law fitting to all lean flame data (i.e., ignoring potential stretch restrictions) produced large fit residuals, an indication of poor fit quality. An alternative, as described below, is to use surface fitting to report  $S_u^0$ s at  $(T_u, P)$  conditions near those realized experimentally, e.g., 400 K and 304 kPa.

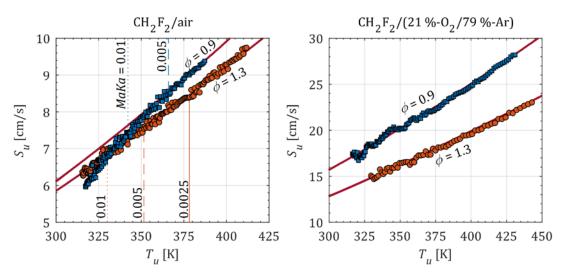


Figure 4: Comparison of lean and rich experimental  $S_u$  values assuming adiabatic conditions with  $P_i = 101$  kPa for (left) CH<sub>2</sub>F<sub>2</sub>/air and (right) CH<sub>2</sub>F<sub>2</sub>/(21 %-O<sub>2</sub>/79 %-argon) including projections of fitted  $\widehat{S_u}$  (thick red lines). Vertical line annotations on the left plot show the calculated locations of different stretch conditions.

Since the values of Ma used to eliminate stretch-affected data were a rough estimation based on propane, it is of value to explore stretch effects further. The importance of stretch can be reduced by using argon inert instead of nitrogen at the same reactant concentrations. Using argon modestly reduces  $\alpha$ , which affects the mixture Lewis and Karlovitz numbers, but also substantially increases experimental  $S_u$  and K. Since  $Ka \sim K/S_u^2$ , the overall result is reduced Ka, and therefore MaKa, compared to flames in air. Experimental  $S_u$  for CH<sub>2</sub>F<sub>2</sub>/(21 %-O<sub>2</sub>/79 %-argon) mixtures with  $P_i = 101$  kPa and  $\phi = 0.9$  and 1.3 are shown on the right of Fig. 4. Because of the reduced sensitivity to stretch, the empirical stretch-free criterion ( $MaKa \le 0.005$ ) is met by all data for both values of  $\phi$ . Both lean and rich  $S_u^0$  curves closely follow their fitted power law curves, and there is less uncertainty in extrapolating to 298 K and 101 kPa.

The variation of  $S_u^0$  with  $\phi$  is presented in Fig. 5 for flames in air. The lower curves show results for flames at (298 K, 101 kPa) and the upper curves at (400 K, 304 kPa). For each temperature/pressure condition, results are shown for data reduction assuming adiabatic conditions (ADI) and assuming radiative heat losses at the optically thin limit (OTL). At (298 K, 101 kPa), the OTL  $S_u^0$  values are about 17 % higher than ADI values, while for flames at (400 K, 304 kPa), the OTL  $S_u^0$  values are 17 % to 23 % greater than the ADI values. For comparison, the data of Takizawa et al. [33] are also presented (x

symbols), and these agree well with the present data reduced with the adiabatic model (which was the same assumption used in Ref. 33). Data from Moghaddas et al. [37] are also presented at (400 K, 304 kPa), and these agree with the present ADI data and those of Ref. 33 for  $\phi \ge 1.2$ , but are higher as  $\phi$  decreases. Reasons for this remain unclear, although differences in stretch correction or in data reduction techniques are possibilities.

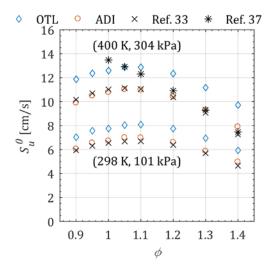


Figure 5: Comparison of experimental  $S_u^0$  values for  $CH_2F_2$ /air flames obtained with adiabatic (ADI) and optically thin (OTL) thermal radiation models along with literature values.

## 5. Concluding remarks

Burning velocities of difluoromethane/air and difluoromethane/oxygen/argon flames were measured in a constant volume, outwardly-propagating, spherical flame experiment, with initial conditions near ambient and for equivalence ratios from 0.9 to 1.4. Data reduction of the measured pressure traces was analyzed to understand the effects of burned gas thermal radiation and flame stretch. For unburned gases at 298 K and 101 kPa, modeling the burned gas thermal radiation at the optically thin limit increased the inferred burning velocities in air by about 17 % compared to those inferred with an adiabatic model. This was due to reduced burned gas expansion velocity and greater total flame front velocity when including the radiative heat losses. More sophisticated, and potentially more accurate, radiation reabsorption calculations require infrared absorption spectra data at combustion-relevant temperatures and pressures which are not presently available. The role of flame stretch on burning velocity was parameterized by the product of Markstein and Karlovitz numbers. The data for stoichiometric and rich flames was estimated to be essentially stretch-free for most of the conditions presented, however, lean flames may be influenced by stretch at smaller radii. Moreover, producing laminar burning velocities at unburned gas conditions of 298 K and 101 kPa from power law surface fits to the experimental burning velocities requires extrapolation which introduces larger uncertainty. In contrast, interpolating measured burning velocities to 400 K and 304 kPa avoids uncertainty due to extrapolations and may provide better quality data for kinetic model validation. To facilitate accurate assessment of refrigerant flammability and provide data suitable for kinetic model development and optimization, data reduction procedures used to generate experimental burning velocities should be scrutinized.

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