

# Towards Consensus Standards for Reference Data for Biofuels

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Standards and Measurement Needs for New Transportation Fuels
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### **Themes of Discussion**

- Who needs property data? Why?
- Historical parallels
- What's being done? Future Plans



## **Stakeholders in Properties Issues**

### Properties for Production, Distribution, and End Use

- Design/Optimization involving processing, refining, distilling
- Innovative design of equipment (e.g. engines, including operating parameters)
- Blending Optimization
- Policymakers (measures of sustainability)
- Legal Metrology
- Operations involving processing, refining, distilling



## **Conclusions of Workshop (2008)**

...better knowledge of fuel properties would lead to better designs and shorter development times of everything from production facilities to emissions control systems."



urface



# Importance of Properties (Uncertainties)

#### **Plant Operations**

Some rough rules of thumb. For a \$1M operation:

- 1% uncertainty in density costs \$10k
- 1 % uncertainty in phase boundary costs \$100k
- 1 % uncertainty in viscosity costs \$1k

Source: K.R. Cox, Fluid Phase Equil. 1993 A.H. Larsen, Fluid Phase Equil. 1986

#### **Custody Transfer--gas pipeline system**

Vendor 1: sells at p1, T1, {x1} Vendor 2: sells at p2, T2, {x2}

Buyer purchases resultant mixture at p3, T3, {x3}

Auditor discovers \$1M per day discrepancy in transaction.



# Thermophysical Properties

# Lessons Learned from Replacement of the CFC Refrigerants

CFCs phased out by regulation (Montreal Protocol—1987)

Established industries/infrastructures challenged

Potential alternatives proposed/discussed

Problems with direct drop-in replacements
(e.g., R11 replaced by R123 in chillers—15 % efficiency penalty)

Properties studied, consensus data achieved (IEA Working Group), designs reviewed, innovation/optimization succeeded



#### Result:

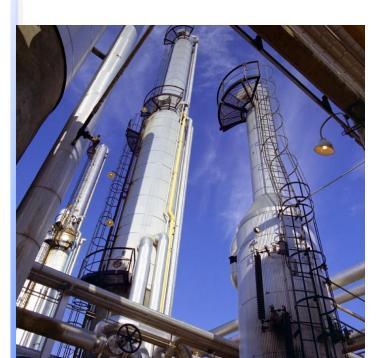
For R123 - 20 % improvement in energy efficiency.

For U.S. refrigeration industry (R134a) - 60 % improvement in efficiency and large operating cost savings.

(About \$50B/yr or 10 EJ per year for all vapor compression equipment in US)



# Historical Antecedent: Petrofuels



Petroleum property data efforts: circa 1916 (NBS, Bearce & Peffer)

Coordination of data needs: 1942, API Project 44

Data inadequacies noted 1972, new API data effort

Petroleum measurement tables: 1980

International consensus: ASTM D 1250; API 2540, IP 200 (ADJD 1250CD)

(Adjunct to D1250-04 Temperature and Pressure Volume Correction Factors for Generalized Crude Oils, Refined Products, and Lubricating Oils)

Refinery data needs: 1980's, 1990's

Petrofuel & petrochemical plants: designed & operated under plant simulation software—based on one century of thermophysical properties data.



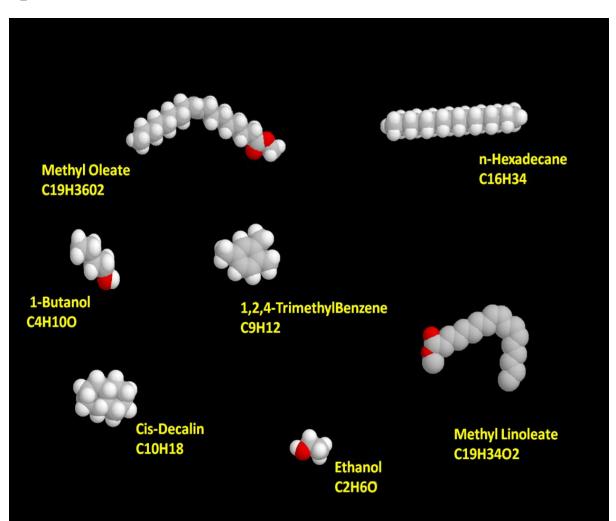


#### **Biofuels: So What's Different?**

These have different molecules, with differing polarity, reactivity, oxygen content, associative and hydroscopic "parameters," ....

#### What we're told:

- •Old "rules of thumb" do not apply
- Data situation is not adequate
- Models are inconsistent

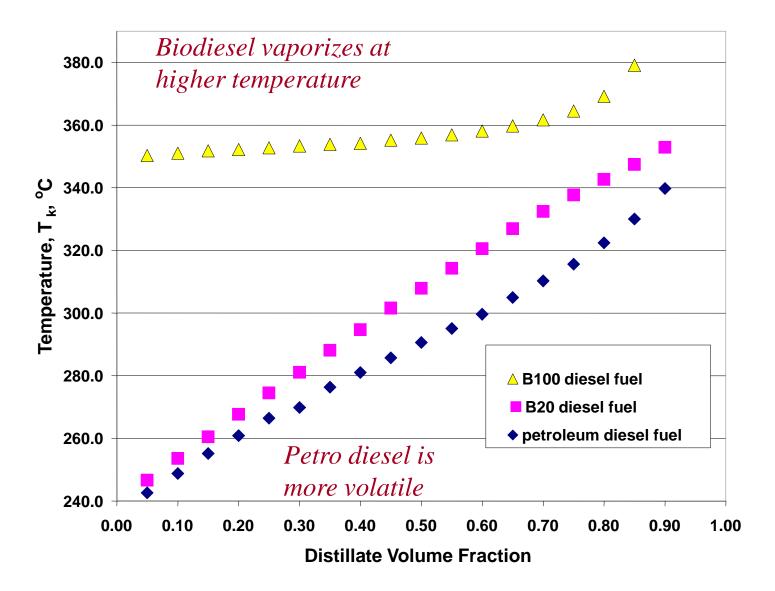








### **Distillation Curves**

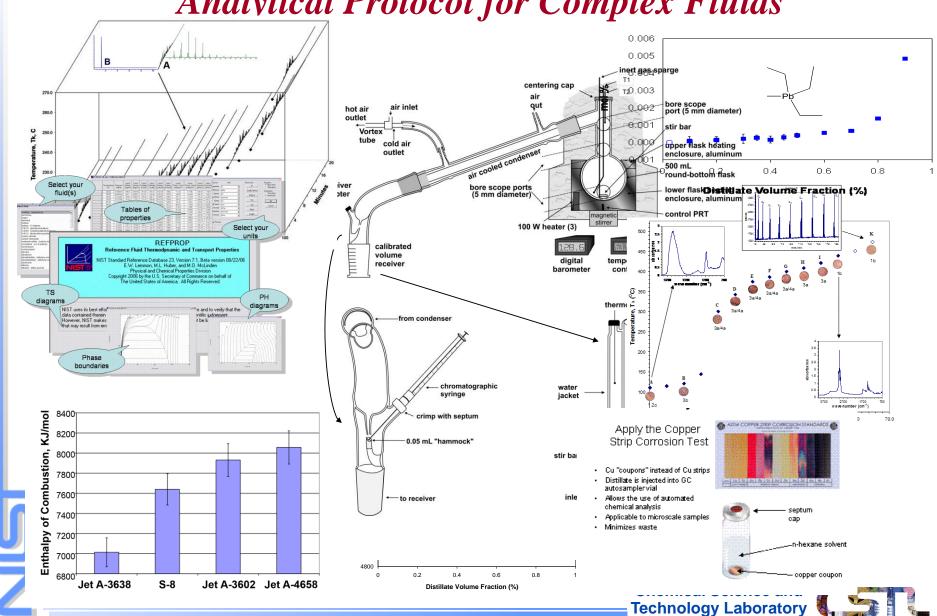






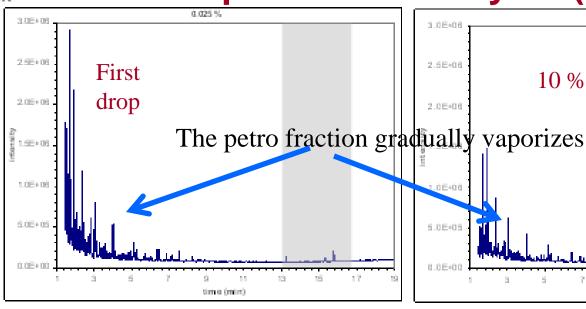
### **Advanced Distillation Curve**

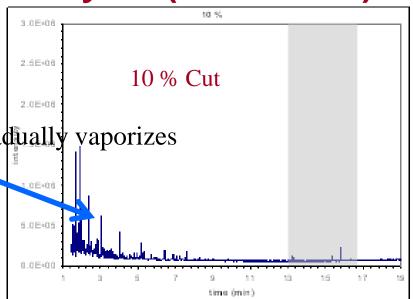
Analytical Protocol for Complex Fluids

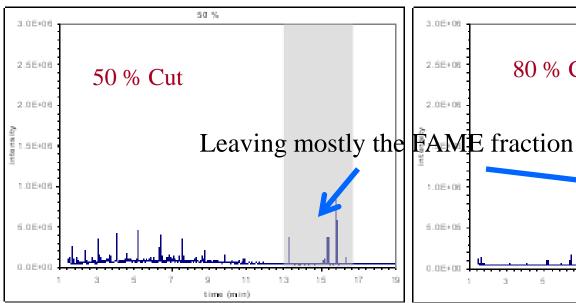


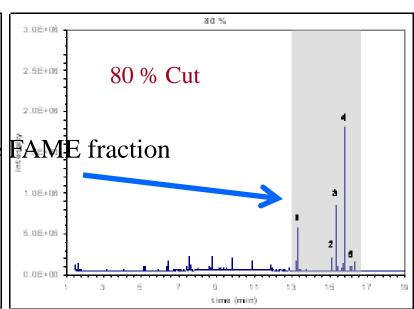
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**B20: Compositional Analysis (GC Traces)** 









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#### **Advanced Distillation Curve**

Analytical Protocol for Complex Fluids



- Temperature, volume and pressure measurements of low well as the round-bottom flask trainty - EOS development

- Composition explicit data charmel for qualitative, quantitative and trace analysis of fractions

- Energy content of each fraction
- Corrosivity of each fraction
- Greenhouse gas output of each fraction
- Thermal and oxidative stability of the fluids
- Temperatures are true thermodynamic state points

Bruno, T. J et al. Anal. Chem. 2010, 82, 777-783.

(February 2010 feature article)



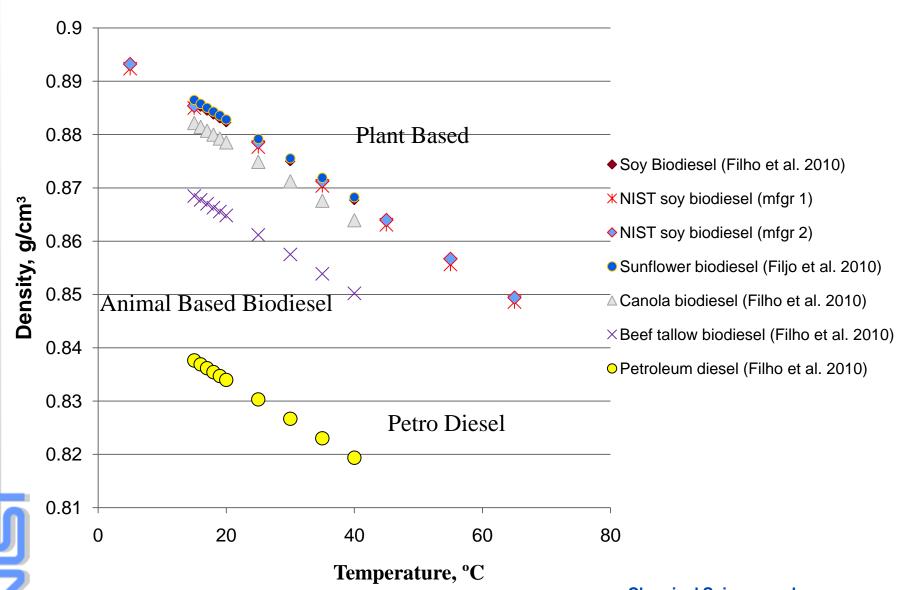
receiver collection

calibrated





### **Biofuel Densities**



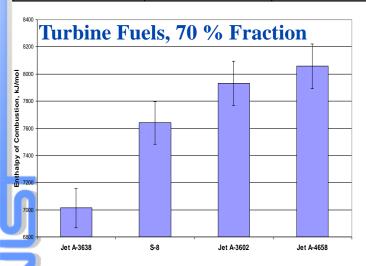
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**Synthetic Fuels: Energy Content** 

# Within-spec alternative fuels can have large differences in energy content!

Composite 1	Basis		
UL94	UL102	100LL	
Petro-alternative	<b>Bio-derived</b>	Standard	
4591 (229.6)	4501 (225.0)	4988 (249.4)	kJ/mol
43.7 (2.2)	42.0 (2.1)	44.4 (2.2)	kJ/g
31.4 (1.6)	33.6 (1.7)	30.7 (1.5)	kJ/mL





# Composite Enthalpy of Combustion, -kJ/g (Biodiesels)

Distillate Volume	SME	CME	B100		
Fraction (%)	Soy	Cuphea	Retail		
0.025	37 (1)	34(1)	36 (1)		
10	37 (1)	34(1)	36 (1)		
50	37 (1)	34(1)	36 (1)		
80	37(1)	37(1) Science and	37 (1)		

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## How to Describe Fuels: Surrogates

#### Petroleum based diesel

- **Alkanes**
- n-hexadecane (straight chain)
- 2-methyltridecane (branched)
- Naphthenes (cycloalkanes)
  - Butylcyclohexane (one-ring)
- Cis-decalin (two-ring)

- Aromatics
  - -1,2,4-trimethylbenzene (one-ring)
  - –1-methylnaphthalene (two-ring)



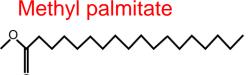
- Naphtho-aromatics
  - tetralin



**Fatty-acid methylesters** 

Methyl stearate

Methyl palmitate



Methyl oleate

Methyl linolenate

Methyl linoleate





## **Are Adequate Data Available?**

Com	Total Nur poun <b>®Nam</b> e	Tot		rhautá	Critical Parameters	Transition Properties	Vapor Pressure	Density	Heat Capacity	Other Properties	T	otal
octane	90000	, I	Costa Po	ints 18	46	123	719	2619	532	2145	6	184
hexade	cane		C <sub>16</sub> I	H <sub>34</sub>	9	118	215	807	242	774	2	165
ethanol	70000		C <sub>2</sub> F		1 <b>60</b> itano	ol 34	1877	3833	1457	580	98	323
1-butan	<b>ol</b> 60000			I <sub>10</sub> O	31	17	1226	2586	5-2	48	57	768
methyl	myristate			$H_{30}O_2$	0	25	123	25	6	13	3	31
methyl <sub>l</sub>	palmitate		Ç <sub>007</sub>	$H_{34}O_2$	0	mayethyl	limgeate	20	2 )5	13	4	69
methyl l	30000 linoleate 20000		<b>©</b> <sub>99</sub> l	H <sub>34</sub> O <sub>2</sub>	0	11	22	9		9	6	66
methyl	oleate 10000		<b>©</b> ှု	H <sub>36</sub> O <sub>2</sub>	0	5	66	45		17	1	79
methyl	octadecano	ate	ල <sub>19</sub> I	H <sub>38</sub> O <sub>2</sub>	0	4	21	2	4 -	14	3	62
methyl	arachidate		$C_{21}$	H <sub>42</sub> Os	1 <b>0</b> 85	199 <b>20</b>	995 <b>34</b> 2	000 1	200 <b>104</b> 2	009 <b>O</b> Yea	ır 1	75

Experimental Thermophysical Property Data: Pures, Binaries, Ternaries, Total





# How to Obtain Properties: "Data on Demand"



□Software tools for mass-scale data capture



□Comprehensive Data Storage Facility



□ Data Entry Facility



□ Data Communications Standard



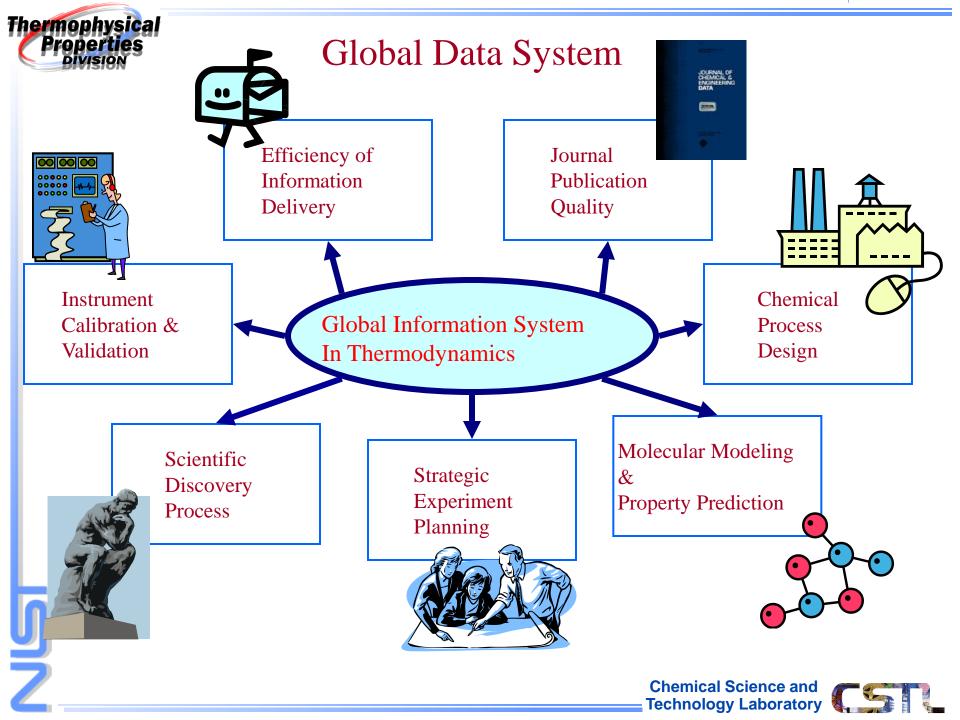
☐ Data Reader Software



☐Software Expert Systems



☐ Web Communication Portal





# Goals for Program on Biofuels Reference Data

To facilitate international trade in the technologies, innovation in design, optimization of plants and components, rational choices among alternatives, and transparency in the marketplace, we should strive for global consensus on fuel property data. This requires:

- Standards for communicating data and models for fuels
- Comprehensive experimental data
- Property models for
  - constituents of biofuels (intermediates, waste streams, etc.)
  - finished fuels
  - blends of biofuels with conventional fuels
  - blended fuels with additives







### The Path Forward: What Must be Done?

- Analysis of the properties most important for engine analysis, process design, pipeline transport, etc.
- Compilations of literature data
- Evaluations of data
- Experimental measurements
- Development of thermodynamic and transport property models
- Evaluation of thermodynamic and transport property models, leading to the declaration of international standards

Proposal for Discussion: *Establish international working group to foster coordination and cooperation in these efforts.* 





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QUESTIONS???

